

Proceedings of the Mid-Term Assessment Workshop of the European Integrated Hydrogen Project - Phase II [EIHP2]



Proceedings Volume 2 *Breakout Session Refuelling Station*

held at the European Commission's
CCAB - Centre Albert Borchette
Brussels, 02 October 2002



Moderators: Henrik Andersen, Christian Machens

- **14:10: “Challenges in development of an infrastructure in Europe - Experience from CUTE ” (M. Jones, BP)**
- **14:30: “Development of a Code for H2 Vehicle Refuelling Stations” (J. Barron, Shell)**
- **14:50: “Hydrogen Filling Station Based on Water-Electrolysis” (Ch. Machens, Vandenborre Technologies)**
- **15:10: “Hydrogen Filling Station Based on NG Reforming” (H. Andersen, Norsk Hydro)**
- **15:30: “Liquid Hydrogen Filling Station” (L. Allidiers, Air Liquide)**
- **15:50: “Gaseous Hydrogen Filling Station” (P. Bout, APCI)**
- **16:10: General discussion and formulation of conclusions/findings**



Session notes and remarks by Dr. Jeff Seisler, ENGVA

A variety of fuelling options for hydrogen were presented and discussed.

These included:

- Hydrogen fuelling on existing petrol stations
- Hydrogen station based upon water electrolysis
- Hydrogen filling station based on natural gas reforming
- Liquid hydrogen filling station
- Gaseous hydrogen filling station



There were several issues that are similar for each of the options on fuelling stations:

- First cost of the station. Electrolysis would add about kEuro.400-500 for a station that would have a compressor installed (such as might be for CNG). Current natural gas reformation technology also would add about kEuro. 400-500 to a normal compressor station (based on CNG). One element cost reduction relates to economies of scale; another will relate to fuelling station design strategies. Both of these will be important among the options that were discussed.
- Building codes and fire codes are of concern, for physical distances that are required between equipment, habitation areas, compressors, storage, etc. These affect the cost of fuelling stations, the design, and the areas (downtown; rural) that stations can be installed.



There were several issues that are similar for each of the options on fuelling stations (cont.'d):

- Size of 'footprint'. Many of the fuelling station systems are large (i.e. package compressor system with electrolysis ~ 15 metres long). If the equipment is too big, it will not fit into areas in more congested urban areas.
- Transport of the fuel is an important issue. Cryogenic fuels (LNG, LH₂) carried by truck increase in cost as the distance travelled increases. Truck transport of gaseous fuel is challenging because the lack of energy density decreases the fuel capacity of a truck or train. The economics and physical aspects of such transport are important.



Remarks:

One thing that was not mentioned that I think is going to be important is for hydrogen vehicles (unlike NGVs): H₂ vehicles will be dedicated (H₂-only) vehicles. The penetration rate of fuelling stations is going to have to be much more significant and widespread and quicker to satisfy the fuel needs of growing numbers of drivers. With CNG, we can 'suffer' through having less concentration of stations because many of the vehicles are bi-fuel and can use petrol as well. Thus the rapid need for high volumes of stations is diminished, thus elongating the time, and thus the economics/costs of building the fuelling infrastructure. In turn this situation affects the overall strategy as to which customers are approached: fleets only; commuters; or some combination. This would make for an interesting study for both natural gas and hydrogen, both gaseous and cryogenic.

As I said in my closing statement, the future is a big place. It's going to take a long time to get there and the trip is going to be expensive.



Mid-Term Assessment Workshop

Brussels
02 October 2002

Breakout Group Sessions
WP2 Presentation by:
James Barron

Hydrogen Vehicle Refuelling Stations



Development of a Code for Vehicle Refuelling Stations

WP2 Group Objective:

- **Develop code for CGH2 refuelling stations as first priority:**
Supply sources of H2 Hydrogen:
 - On-site generation eg electrolyser, reformer
 - 'Trucked-in' CGH2 or LH2; pipeline
- **Develop code for LH2 refuelling stations as second priority**
- **Codes to be recommended to become ISO Standards**



Scope of Code: CGH2 Vehicle Refuelling Stations

Main Plant Components:

- **Compression system**
- **Buffer storage system**
- **Dispenser to hose refuelling nozzle**

Contents of Code:

- **Design (including installation on existing service stations)**
- **Hazardous areas and zones, isolation distances**
- **Construction**
- **Operation and Maintenance**



Reference Documents considered in preparation of Draft

- **ELGA Document 15/96: Gaseous Hydrogen Installations**
- **NFPA 50A: Standard for Gaseous Hydrogen systems at Consumer Sites**
- **German TRG 406 (Draft): CGH2 Refuelling Stations**
- **ISO 15916: Basic considerations for the safety of hydrogen systems**



Progress plan for development of CGH2 Code

- Draft prepared & circulated to WP2 Group (August 2002)
- WP2 Group meeting held 18 & 19 Sept 2002 in Amsterdam to discuss Draft
- Review of Hazardous areas, zones & isolation distances also referred to WP5 Group for comment on selection & determination
- WP2 Group meeting 2 Oct 2002 in Brussels to discuss follow-up action items arising from meeting on 18 & 19 Sept 2002
- Target to complete Drafts within EIHP2 Project duration





EIHP2 Mid-Term Assessment workshop Brussels, 02nd Oct. 2002

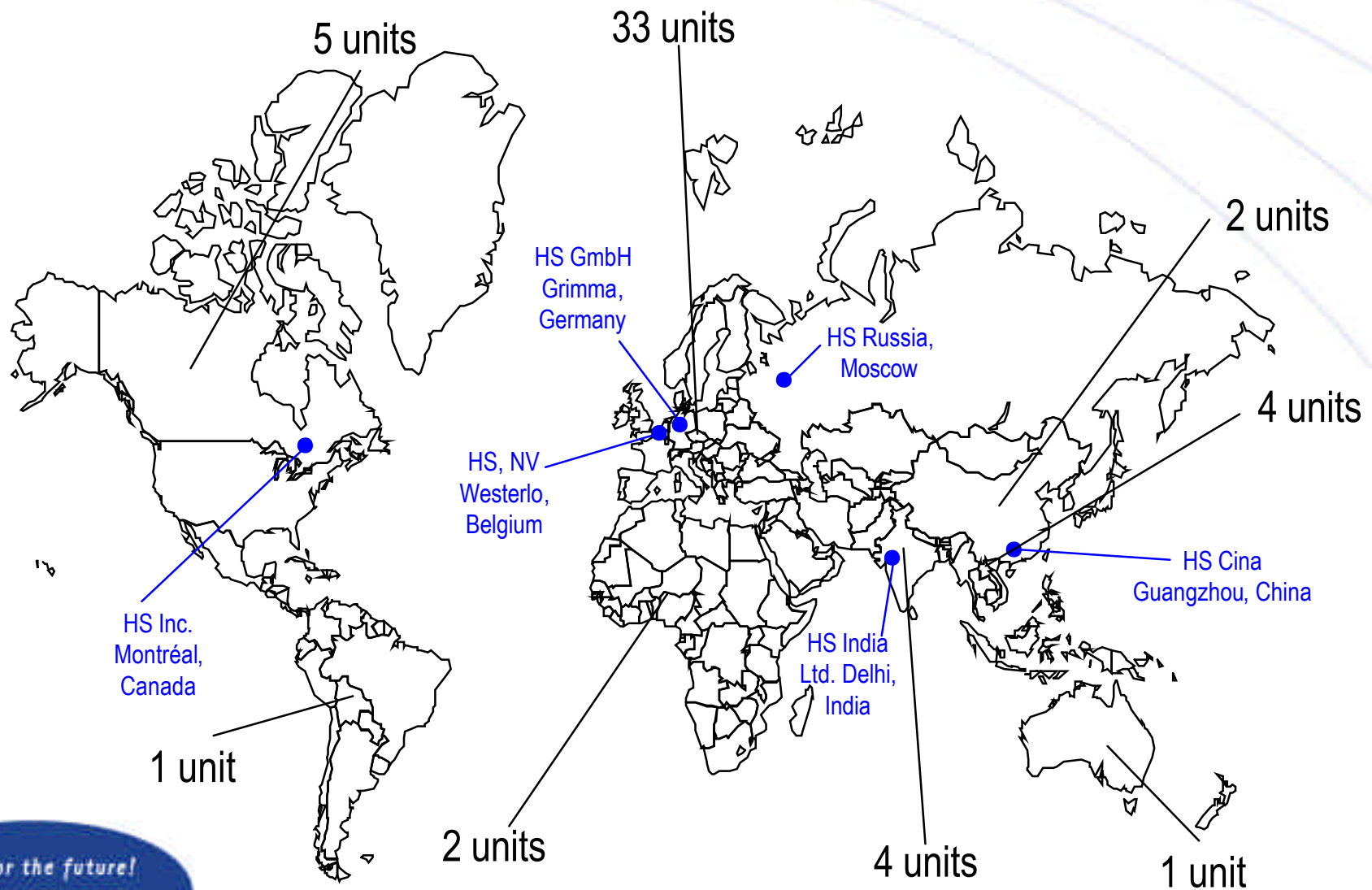


„Hydrogen filling stations based
on water electrolysis“

by

Christian Machens

Worldwide locations and units in the field





What is a filling station ?

- Location where vehicles (FCV / ICEV) can be fuelled with Hydrogen (in this case $\text{CGH}_2 > 200 \text{ bar}$)
- Standardised refuelling procedure
- Standardised safety aspects (Equipment, safety-distances, standards)
- Standardised Product Quality (also P, %, T, RH, ...)
- Standardised metering system
- Standardised maintenance



Overview on standards

	CNG	LNG	CH2	LH2
Gas supply	ISO 15403	NF EN 1160 PREN 1532 PREN 13645 EN 1473	ISO 14687 ISO WG 7 ISO WD 15916	ISO 14687 ISO WG 7 ISO WD 15916 ISO WG 2 ISO/WD 13986
Refuelling Station	PREN 13638 EN 13423	NFPA 59 A NFPA 497	ISO WG 4	WG 3 ISO WG 15594
Dispenser metering	Under construction by OIML			
Vehicle installation	Regulation 110 ISO 15501	NFPA 57 SAE 2323 SAE J2343		
Vehicle cylinder	ISO 11439	EN 1251 EN 1252 EN 12213 EN 12300 PREN 12456	ISO WG 6 ISO 15869	ISO WG 1 ISO 13984 ISO 13985
Vehicle refuelling coupling	ISO FDIS 14469	No standard available	ISO WG 5 ISO/AWI 17268	
Vehicle Components	ISO 15500	NF EN 12065 UNE EN 12066 UNE EN 12308 NF EN 12567 EN 1626 EN 1797 EN 12434		

Source: Ballast Nedam

Filling station for Compressed Gaseous Hydrogen (CGH₂) produced on-site by water-electrolysis:

(CUTE standards)

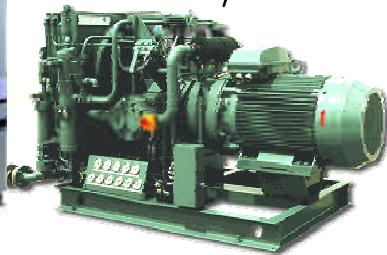
Electrolyser -> Compressor -> Storage ->Dispenser

(25 bar)



ISO 197

(345 bar)



ISO 197

(300 bar)

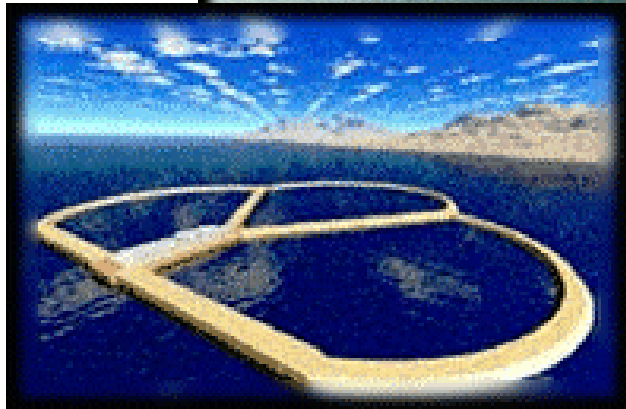


ISO 197

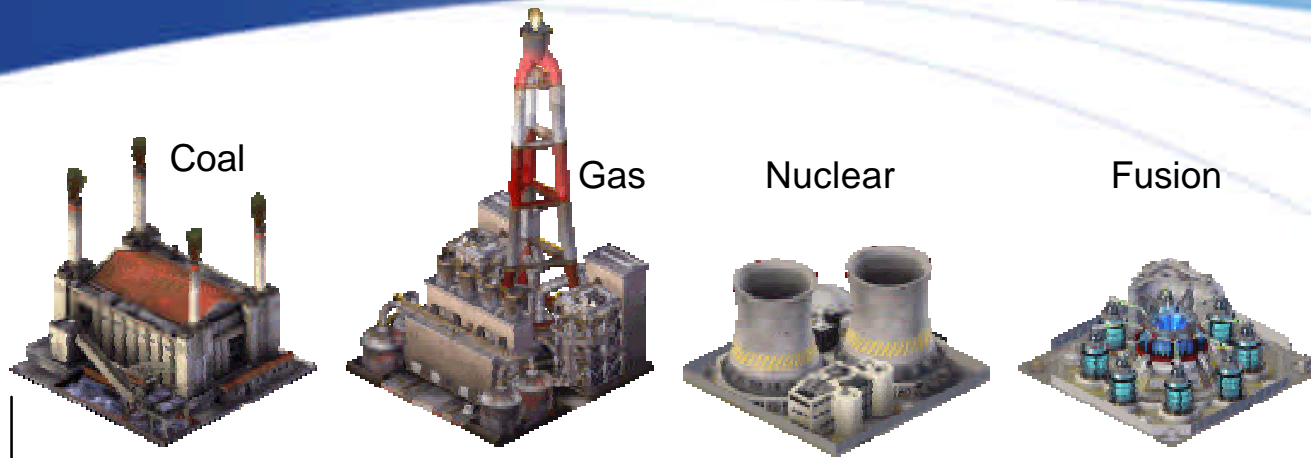
(> 200 bar)



ISO 197



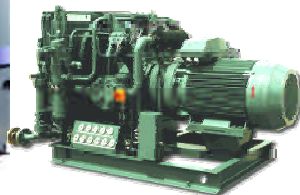
Only water – electrolysis can
produce H₂ without pollution !



Peakshaving surplus power use



Only water-electrolysis can make use of surplus electric power caused by power stations



FCV / ICEV





To be achieved:

- Development of specific standards for on-site production
- More demonstration projects (e.g. CUTE)
- Information to the public
- Legislation to ensure support of H₂ – vehicles
- Acknowledgement of H₂ as a fuel

Mid-Term Assessment Workshop

Brussels
02 October 2002

Breakout Group Sessions
WP2 Presentation by:
Henrik Andersen – Norsk Hydro

Natural Gas Reforming



- Quality
 - H₂ quality
 - Appearance
- Safety
 - Build-in safety features
- Environment
 - Emissions
- Cost
 - Efficiency
 - Compactness



NG Reforming – Efficiency

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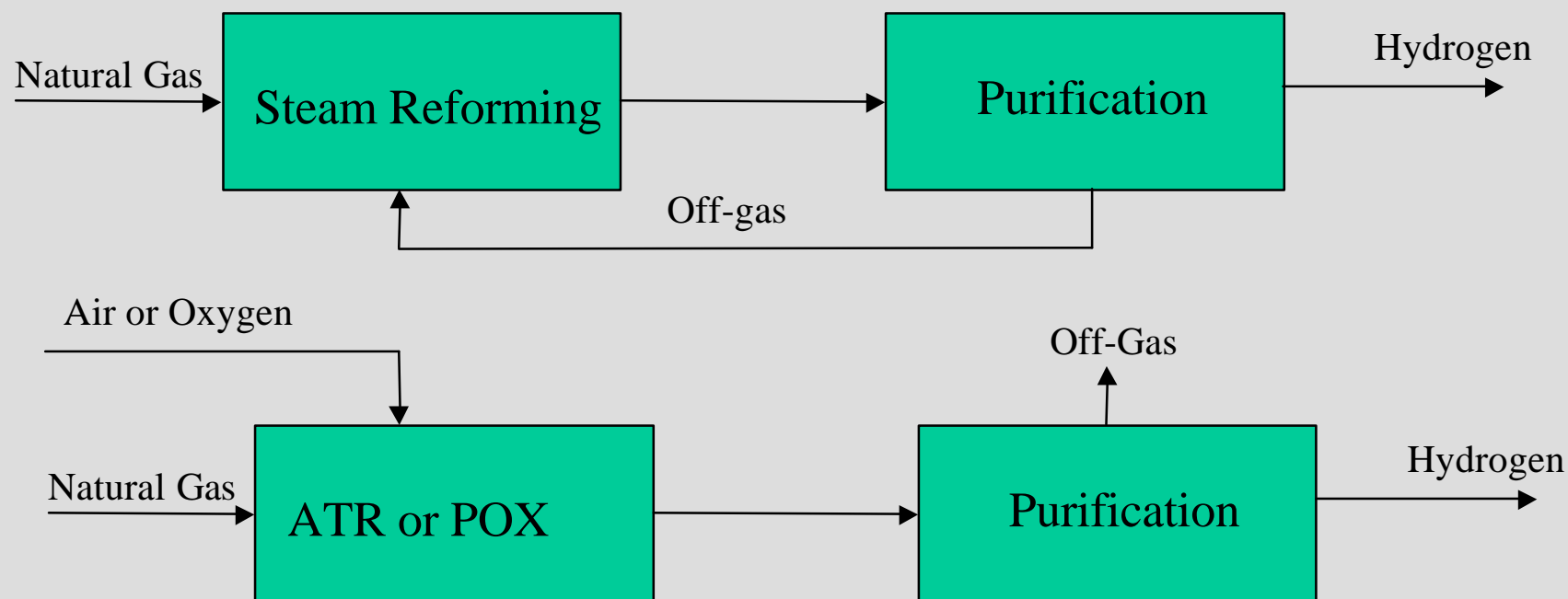
Reforming : $\text{CH}_4 + 2\text{H}_2\text{O} = 4\text{H}_2 + \text{CO}_2$;	0.4 Nm ³ NG/Nm ³ H ₂
Electrolysis : $\text{H}_2\text{O} = \text{H}_2 + 1/2\text{O}_2$;	4.0 kwh/Nm ³ H ₂

- NG reforming : 75-80% (HHV)
- Water-Electrolysis : 80-85% (HHV)
 - Power production from natural gas : ~ 50% (HHV)
 - Total chain-efficiency: 40-45% (HHV)



NG Reforming – Technology diversity

4



NG Reforming – Public Acceptance

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- From Industry to the Public



- Preferred purification technology is PSA (Pressure Swing Adsorption)
 - Efficiency, cost and size is a function of H₂ quality



Hard Targets:

- CO below 2 ppm
- CH₄ below 1 ppm
- Inerts below 0.5%



NG Reforming – Emissions

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Emissions	Steam Reforming	ATR
To Air	NO _x Steam CO ₂	Offgas: CO ₂
To earth	Process water Spend catalyst	Process water Spend Catalyst



- Undesired catalytic side reactions
 - Cock-formation
 - Methanisation
- High Temperatures
 - Steam reforming operates at 800-900 deg.C
- Combustion and reaction integrated
 - PSA offgas is used as fuel
 - Sensitive to changes in fuel Wobbe number
- High degree of heat integration
- Sensitive to natural gas quality
 - Sulphur, higher hydrocarbons, CO₂ etc
 - Sulphur deactivates catalyst



Mid-Term Assessment Workshop

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02 October 2002

Presentation by
Laurent ALLIDIERES
Air Liquide
Division Techniques Avancées

LH₂ Refueling Stations



Benefits & drivers for hydrogen fuel

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Environmental benefits: cleaner fuels with less emissions (NO_x, particulates, CO₂...)

- ✓ Local impact: air quality
- ✓ Global impact: limitation of greenhouse gas effect



Diversified energy sources

- ✓ Security of supply
- ✓ Remote energy supply

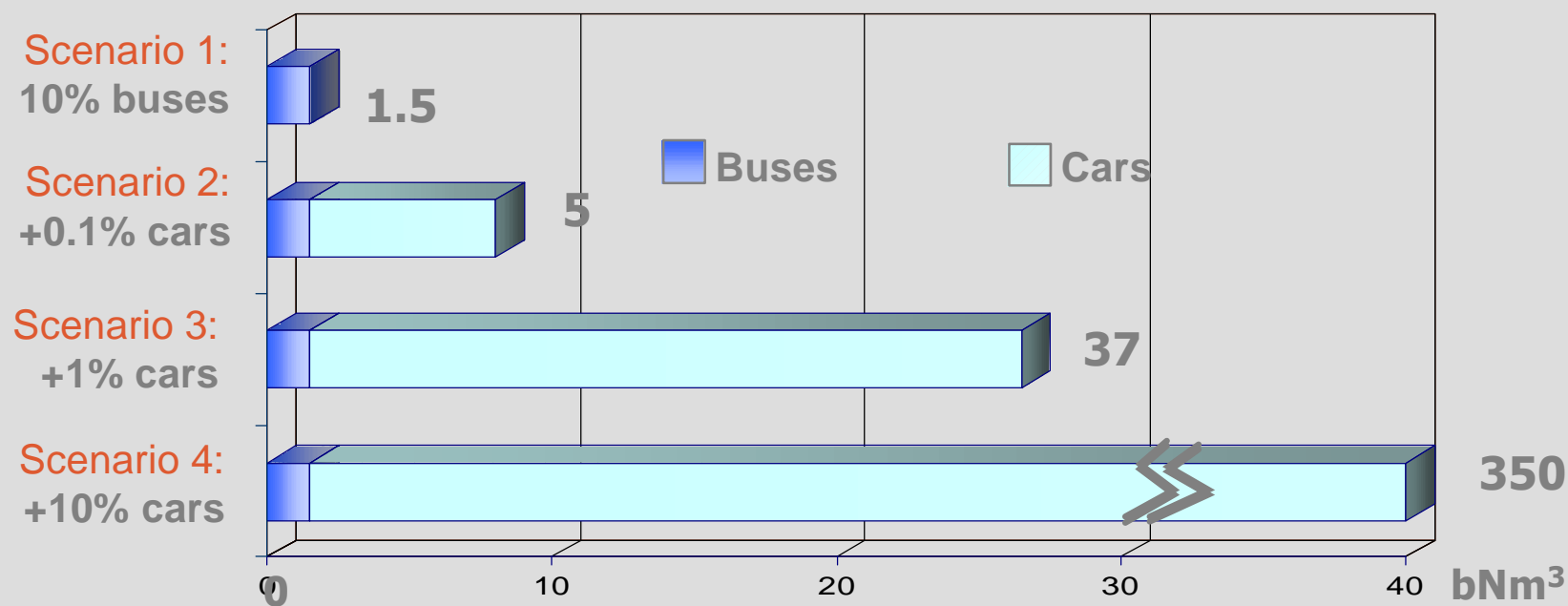
Higher efficiency to improve natural resources utilization

Potential higher efficiency « well to wheel » of fuel cells:

	<u>Well to tank</u>	<u>Tank to wheel</u>	<u>Total</u>
ICE	88%	16%	14%
FC	58%	48%	28%

ICE: Internal Combustion Engine = car FC: Fuel Cell

Hydrogen consumption scenarios for transportation (2010's)

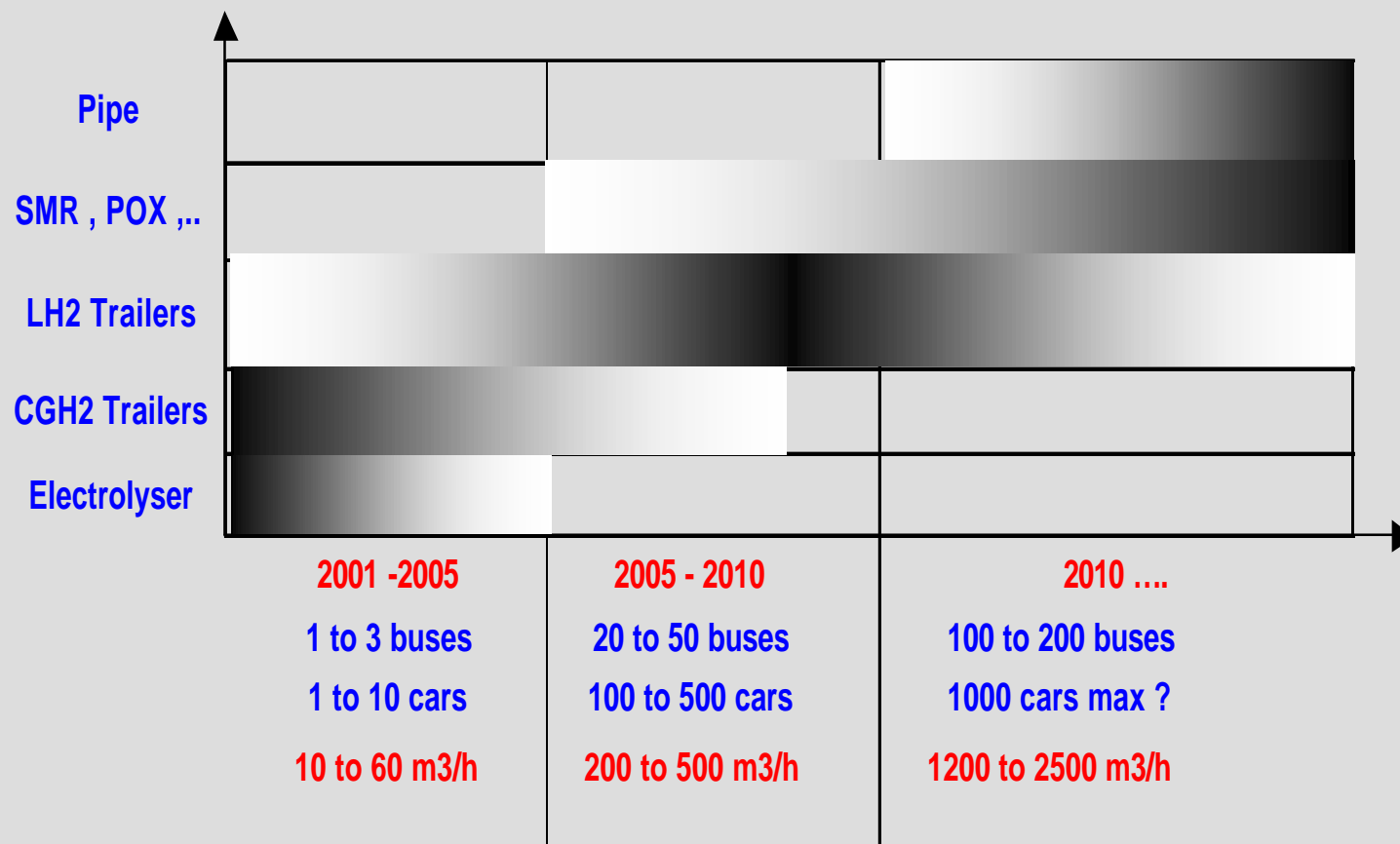


WW energy requirement for transportation : 1600 millions TOE

WW H2 production : 540 bNm³ = 140 millions TOE

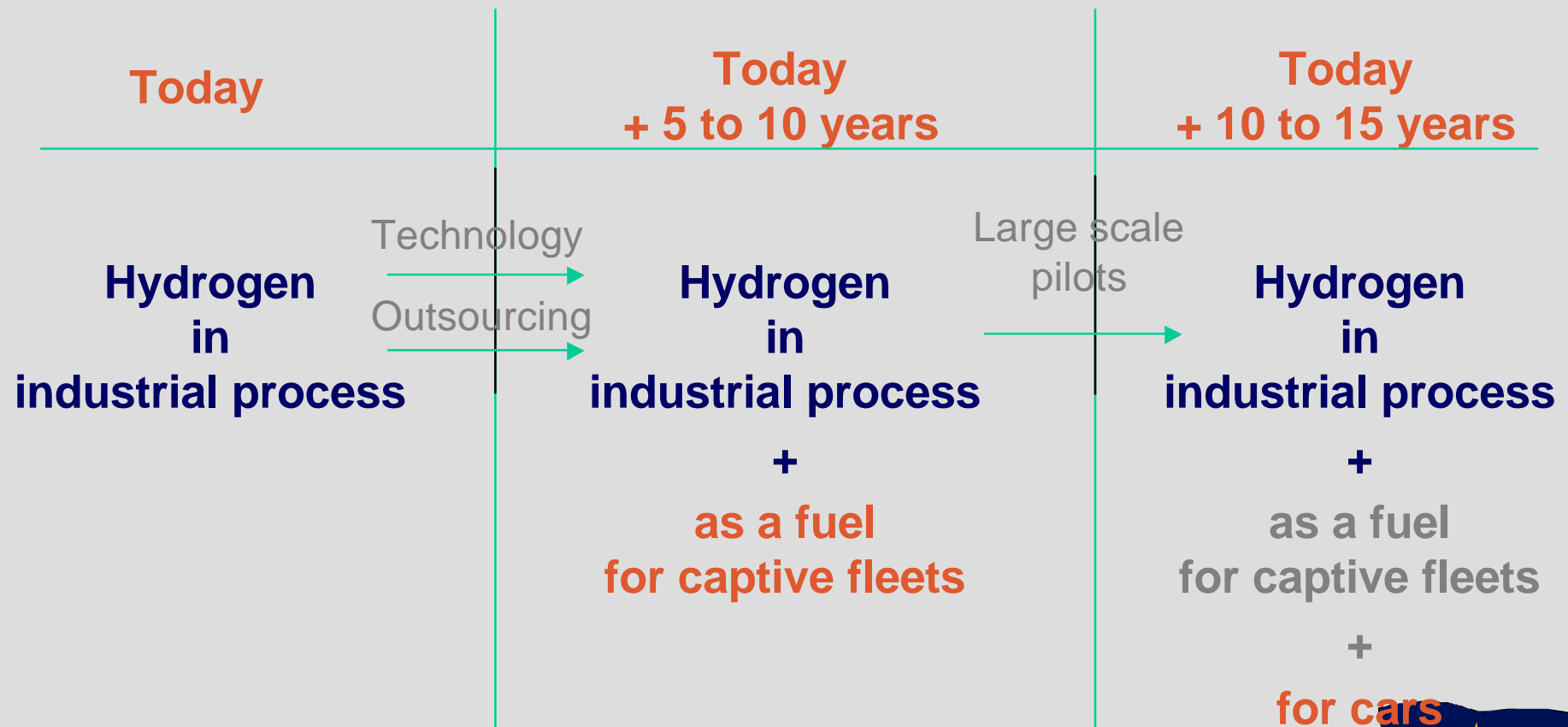
Supply chain scenario (1)

4



Three phase growth model

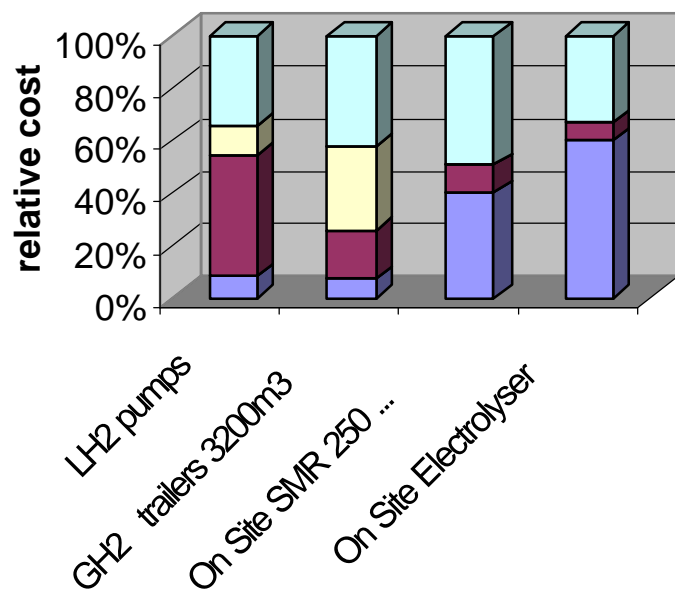
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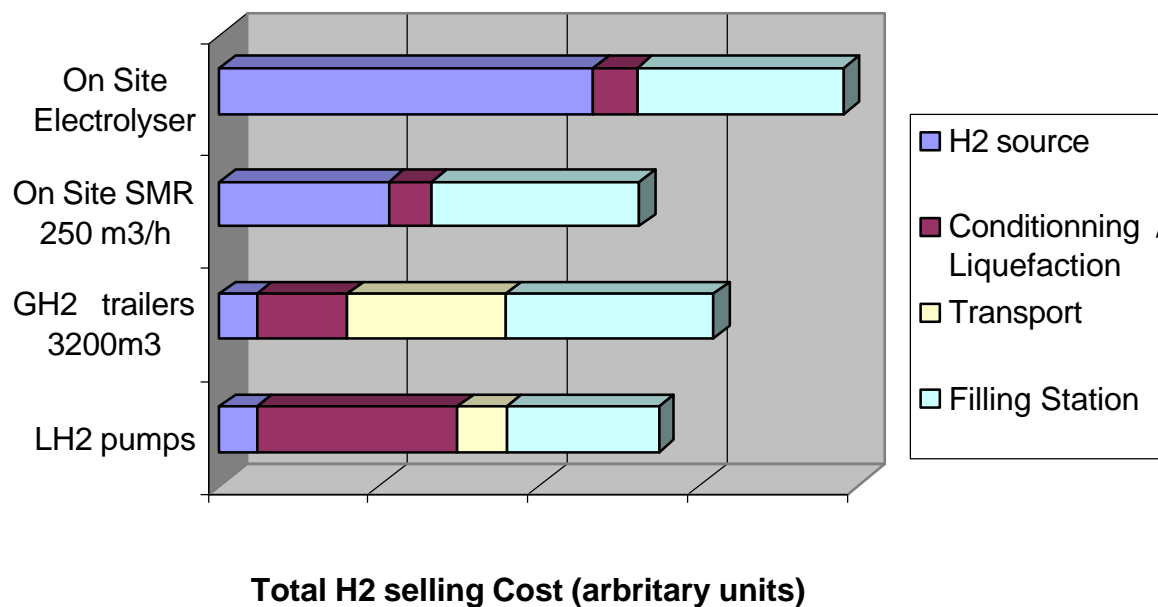
Supply chain scenario (2)

6

Scenario : 20 buses / 250 Nm³/h



Scenario : 20 buses / 250 Nm³/h

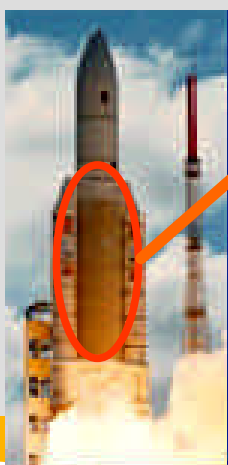


Hydrogen as a fuel for the space industry

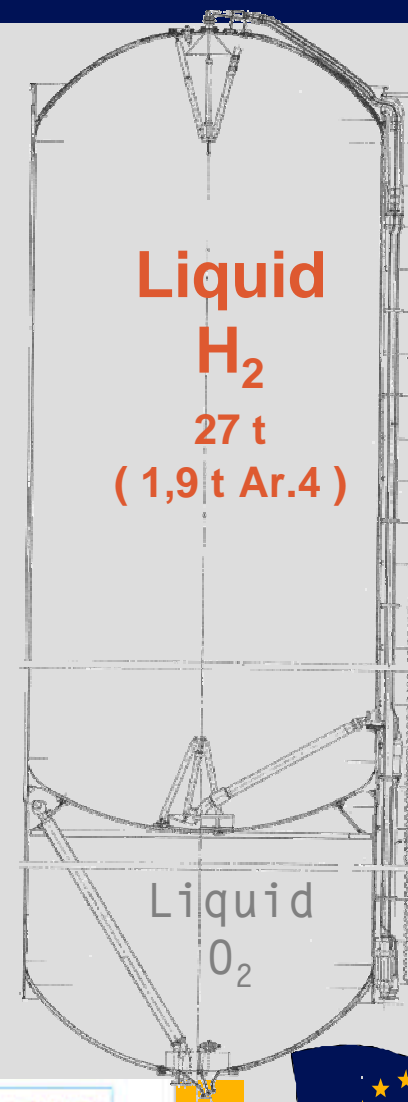
7



Ariane 5 ↓→



- Energy / weight ratio liquid hydrogen
- H₂ reaction with oxygen to provide propulsion



Various scenarios

8

GH₂ source :
pipeline or large SMR > 30 000 m³/h

Liquefaction 10 t/d

Filling center 200 b

On site
SMR or
Electrolysis
250 m³/h

Transport ST LH₂

Transport TT GH₂ 200 b

Refueling Station

- LH₂ tank
- LH₂ pump
- Dispenser

Refueling station

- CGH₂ storage
- Compressor
- Buffer
- Dispenser

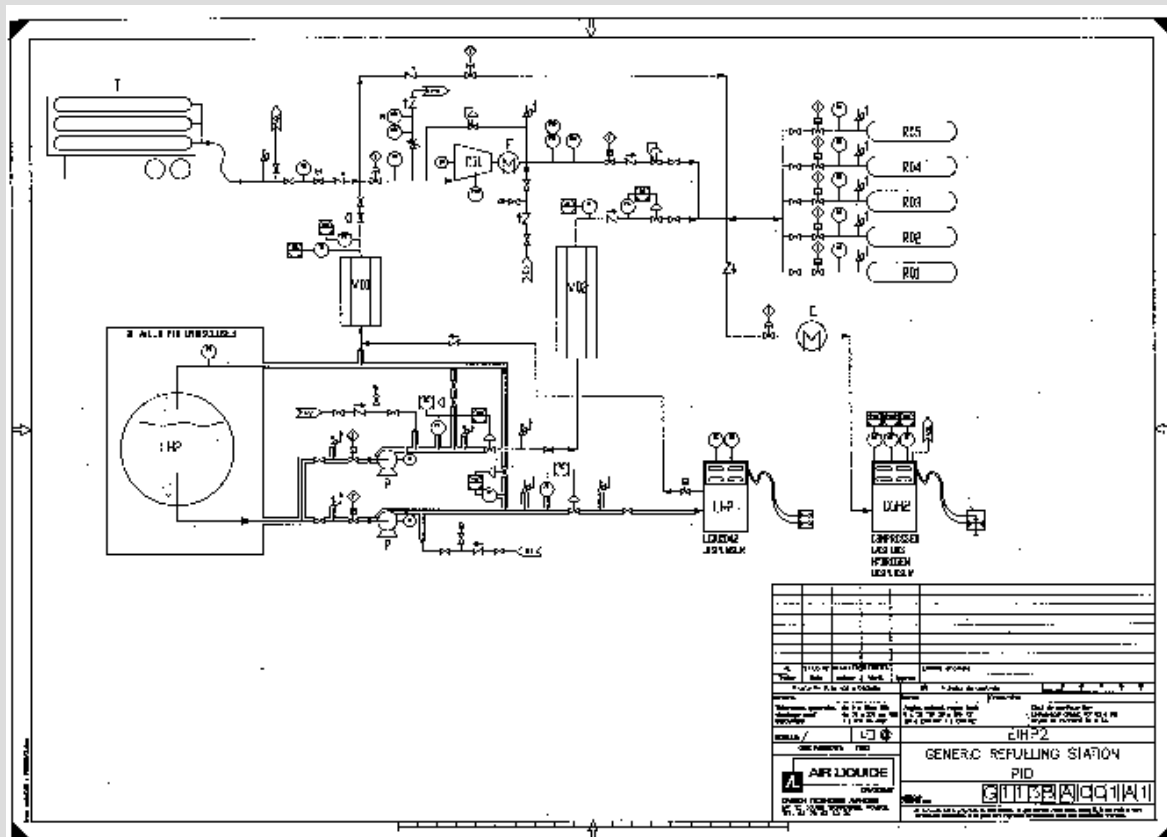
Vaporization



The liquid Hydrogen fuel station concept

9

- LH₂ has a legitimacy in the H₂ well to wheel supply chain scenarios
- A significant advantage is the possibility of having on the same LH₂ supply mode distribution for simultaneous gaseous and liquid dispensers
- This possibility is already illustrated in projects in Munich / Berlin (End 2002) / London (2003) and others.





Current safety distances for LH₂ “stations” in France

- ✓ 8m : No man's land
- ✓ --- 15m : heat resistant material. Enclosure limit
- ✓ --- 30m : “Dangerous area”
- ✓ --- 35m : No Hydrocarbon storage
- ✓ 70m : No public building
- ✓ ...

- « Do not confuse norm and local regulation »
- « We will review EU proposals »
- OK to reconsider safety distances evaluations and new product / technology developments
- Open to underground LH₂ (cryogenic) storages
 - ✓ Not recommended in EN13458 and ISO TC220 : No actual study has been done.
 - ✓ « Natural » protection against vandalism and potential terrorist attacks
 - ✓ Potential opportunity for safety distances reduction

- Review safety studies based on a **VALIDATED** simulation code
 - ✓ Diphasic phase,
 - ✓ Condensation and solidification of air,
 - ✓ Diffusion of H₂ in air / soil
 - ✓ BLEVE
- Dispenser / user interface review must be done
- Continue work on LCGH2 draft for regulation
- One clear challenge
 - ✓ Industrial Hydrogen ⇒ Hydrogen in everyday's life
- **LH2 underground storages**
 - ✓ Safety studies and tests are necessary
 - ✓ Will be done but not within EIHP 2 scope => Middle term development

✓ Air Liquide activities in

✓ Europe

- CUTE and SASSENAGE PILOT PLANT
- PP available for public relation end of this year

✓ US

- Under development

✓ Japan

- NEDO / Tokyo Area

✓ Others

- Cluster activities

✓ Feedback in Y2003

✓ ...



↑ *H2 Testing zone in Air Liquide DTA*



← CGH_2 dispenser
↓ CGH_2 refuelling station



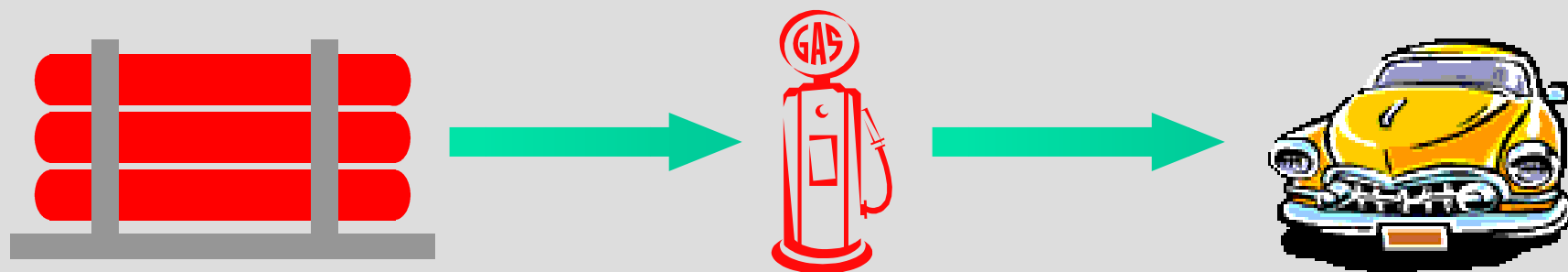
*Technology is more mature
than regulation...*

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Presentation by
Peter Bout





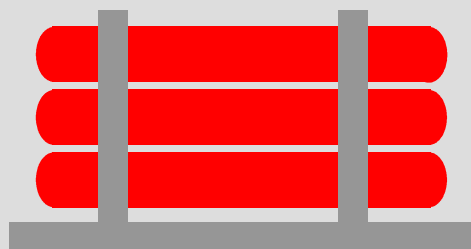
**Production,
Compression &
HP Storage**

Dispenser

**Vehicle
Fuelling**

- | | | |
|--------|--|--------------------------|
| WP 2.2 | Station components to be harmonised | (draft under discussion) |
| WP 2.4 | Introduction of new layouts & technologies | (to be started) |





WP 5

Risk assessment

(preliminary discussions)

Production, Compression & HP Storage

CGH from ~ Electrolysis

~ Reformer

~ Solar

~ etc.

**In general, known applications to
be made suitable for this
application.**





Dispenser



WP 2.2

Station components to be harmonised
(draft under discussion)

WP 3.3

Approval of CGH connector

WP 3.4

Interface with ISO TC197

Issues to be resolved

- **Design considerations**
 - ~ Earthing
 - ~ Leak prevention/detection
 - ~ **Dispenser/vehicle communications** (temperature control)
- b) **Flowmeter**
 - ~ **Accuracy** (wide & rapidly changing pressure range)
 - ~ **Suitable for hydrogen**
- c) **User interface/operation**





Vehicle Fuelling



Issues to be resolved

- **Tank approval**
 - ~ Safety tests & design standards
- b) **Dispensing standards for**
 - ~ Safety distances & training
 - ~ **Fail safe connection** (mechanical & communications)
 - ~ **Fill strategies** (repeatable fills regardless of vender outlet)
- c) **Acceptance by the public**

WP 2.2

Station components to be harmonised
(draft under discussion)

WP 3.2

CGH refuelling procedures

WP 4.5

Approval of components & vehicles

